Hampton Randle

VOC Emissions from Sitka Spruce Lumber

Report to

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Report by

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VOC Emissions from Sitka spruce Lumber

I. Results Summary

One charge containing 73.3 board feet of 2x4 Sitka spruce lumber was dried in a small-scale kiln at Oregon State University. The kiln dry- and wet-bulb temperatures were provided by Hampton Lumber. The dry-bulb temperature was ramped to 165°F (74°C) over 15 hours, then to 180°F (82°C) over 9 hours. The wet-bulb temperature was ramped to 150F (43°C) over 15 hours, then held for the rest of the the drying time. The air velocity was 750 feet per minute (2.5 m/s). The kiln was indirectly heated with steam. There was no humidification. Regulating the amount of air entering the kiln controlled venting and the humidity.

A JUM 3-100 total hydrocarbon analyzer was used to measure organic emissions following EPA Method 25A. It has been demonstrated through past studies (Lavery and Milota, 2000, Forest Products Journal, NCASI/Georgia-Pacific SEP project) that this method in this small-scale kiln gives results similar to a large-scale kiln. The data for the test is summarized in the Table 1.

TABLE 1. Summary of results.

	Carring C	i i o o a i o i			
Charge	Wood	Initial MC	Final MC	VOCa	Time
	Source	%	%	lb/mbf	hrs
1	Randle	70.7	16.1	0.24	48.8

^a To adjust the VOC value to a different final moisture content, add or subtract 0.004 for each percentage point of moisture content difference. The validity of this adjustment is clear in Figure 7.

II. Lumber Source and Handling

Three charges of lumber were delivered to Oregon State University on September 9, 2003, one to be dried and two as a backups. The wood was wrapped in plastic at the mill to prevent predying and loss of organic compounds.

The wood was wrapped and sealed in plastic in packages of 6 to 12 boards and stored at 0°C charges until the charge could be run on November 10. An analyzer problem prevented the drying from occurring when the wood was received.

III. Kiln Description and Operation

A schematic of the kiln is shown in Figure 1. The kiln box is approximately 4' by 4' by 4'. It is indirectly heated by steam. Four dry-bulb thermocouples and two wet-bulb thermocouples are located on the entering-air side of the load. The dry-bulb

thermocouples are spaced in a grid. The two wet-bulb thermocouples are under a single sock at the center of the entering-air side of the load.

Humidity

A 200 L/min MKS mass flow meter controlled and measured the amount of air entering the kiln. It was factory calibrated and checked using a bubble meter. The amount of air entering the kiln is based on the wet-bulb temperature - if it is above setpoint, the airflow is increased and if it is below setpoint the airflow is decreased. This is analogous to venting for a commercial kiln. A minimum of 5 L/min entered the kiln at all times, more than removed by the analyzer (< 1.8 L/min). Putting air into the kiln at a rate of 100 L/min causes the pressure in the kiln to be 60 to 130 Pa above ambient, depending on location in the kiln (high-pressure or low-pressure side). Thus, any fugitive leakage should be out of the kiln. Two additional flow meters can be manually set to provide additional airflow. The steam spray line is disabled, so no water vapor is added to the kiln atmosphere.

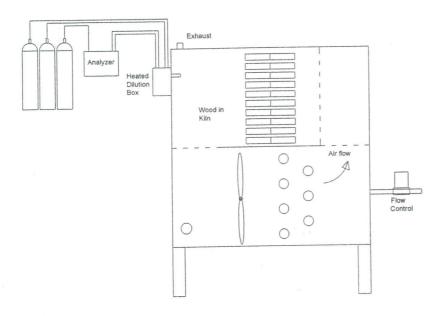


FIGURE 1. Schematic of kiln and sampling system.

Temperature

Temperature in the kiln is controlled by indirect steam heating. When the average of the four dry-bulb thermocouples is below setpoint, the steam pressure in the coil is increased. When it is above setpoint, steam flow to the coil is reduced.

Schedules

The drying schedule supplied by the mill is shown in Table 2. The actual temperatures are presented in Figure 2. The starting temperature was approximately 70°F.

TABLE 2. Drying schedule for charges 1 and 2.

INDLL E. DI	ying ouncaute	101 011011900		
Step time, hours	Ramp time, hours	Dry-bulb, °F	Wet-bulb, °F	
15	15	165	150	
Until dry	8	180	150	

Charge Sequence

The lumber was removed from the freezer and allowed to warm in plastic. The kiln was made ready and 2" were trimmed from each end of each board to give 44" samples. These were then weighed, placed in the kiln, and dried according to the schedule provided. Sampling for hydrocarbon was done as described in section IV. At the end of drying the wood was weighed, oven dried, and reweighed so initial and final moisture contents could be determined by ASTM D4442.

IV. Sampling Systems and Methodologies

Figures 3a and 3b show the hydrocarbon sampling system. The fuel gas was hydrogen. The span gas was EPA Protocol 1527 ppm propane in air, the mid-gas was certified 881 ppm propane. The zero gas was Grade 5 air. Detailed sampling procedures are in Appendix 1 and a summary is presented below.

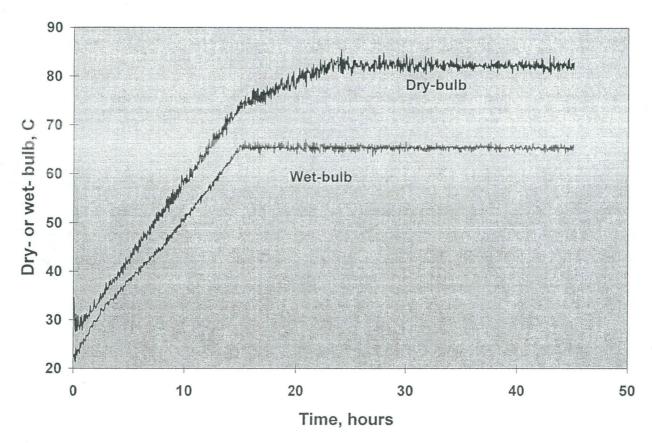


FIGURE 2. Dry- and wet-bulb temperatures during the drying cycles.

The THC sample was drawn from the kiln directly into a dilution/filter box mounted on the side of the kiln. The box was heated to 125°C. It is assumed that the gas in the kiln is well-mixed and that the composition in the kiln near the exhaust is the same at the composition of the exhaust. The sample line from the box to the analyzer was heated to 133°C. The valve at the back of the analyzer was heated to 145°C.

Leak checks were conducted before and after the charge was dried. Valves are closed and all components from just behind the probe tip to the valve at the back of the analyzer are placed under a 19.5 inHg vacuum. Less than one inHg pressure change during two minutes is acceptable and this was met.

Total flow and sample flow to the analyzer were checked using an NIST-traceable flow meter. This was done at the beginning and end of each sampling interval. The meter was attached to the system near the probe tip within the heated box. The valves were repositioned so that the sample came from the meter rather than the kiln. Readings made with the dilution gas off and on indicated the dilution ratio used to lower the gas moisture

content to the detector. The flow readings were verified by observing the change in the analyzer reading for span gas before and after the dilution gas was turned on. The dilution ratio calculated based on the analyzer readings was within 1 to 2% of that determined by the flow meter. Dilution was used when the gas moisture content in the kiln was greater than 15%.

Calibration of the zero and span of the detector was done at the beginning of each run (about every three hours with one eight-hour interval each night). The calibration gas was introduced by setting the valves so the calibration gas entered the system near the probe tip at ambient pressure. The calibration was checked at the end of each run with no adjustments made to the zero or span during the run. The span drift was always less than two percent of full scale for a run and generally less than one percent. The zero drift was minimal during the two days of sampling.

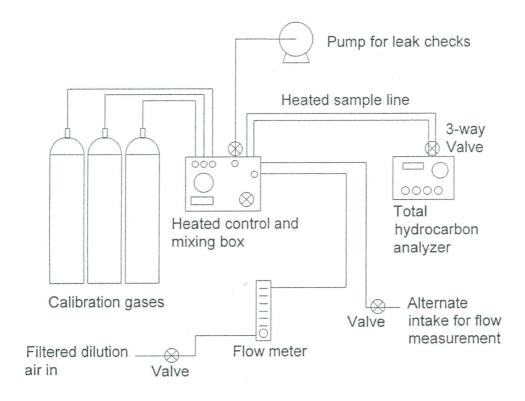


FIGURE 3A. Schematic of heated filter box with air dilution system, heated sample line, and analyzer. Sample enters heated box from back of drawing (box is attached to kiln).

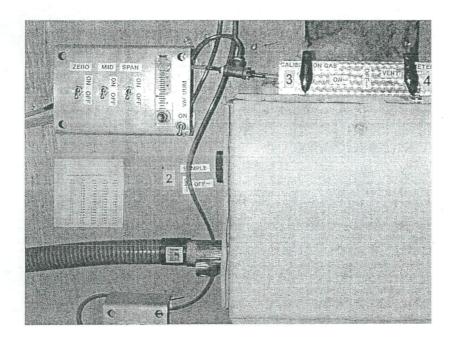


FIGURE 3B. Photo of VOC sampling system showing heated sample box (with white insulation), toggle valves and flow meter for calibration gases (upper left), on/off valve for calibration gas (3 at upper center right), heated sample line to analyzer (green tube, lower left), valve for sample (2 at center), toggle valve to vacuum pump (near calibration gas valves), and vent/flowmeter valve (4 at upper right).

V Data Reduction and Treatment

The "FlowCalc" page in the files "Hampton, Kiln.XLS" in Appendix 2 show the calculations for each 3-minute interval during the charge. Column A is a reading number. Columns B and C are the clock and charge times, respectively. Columns D and E are the average dry- and wet-bulb temperatures. Column F is the vapor pressure at the wet-bulb temperature. The absolute humidity is shown in column G and the molal humidity in column H.

Flow calculations

The volumetric dry gas flow rate in column I (files "Hampton, Kiln.XLS" in Appendix 2) is the flowmeter reading adjusted for the meter calibrations and the molar humidity of the entering gas. This is in standard (at 0°C) liters per minute. In column J this has been converted to a mass flow rate in kg/min and in column K is the same information is expressed as a molal flow rate.

Moisture calculations

The water removal rate in g/min (column L) (files "Hampton, Kiln.XLS" in Appendix 2) is calculated from the humidity and the gas flow rate and the total water (column M) is an integration of column L over time.

The moisture content of the wood at each interval in the event (column N) was determined by reducing the MC of the wood based on the amount of water leaving the kiln during the previous 3-minute interval.

Total hydrocarbon calculations

The original total hydrocarbon analyzer reading is shown in column O (files "Hampton, Kiln.XLS" in Appendix 2). In column P this has been corrected to compensate for the range setting switch on the analyzer and scaling between the analyzer reading and the computer reading. Also in column P, the THA data between sampling runs has been adjusted to the average of the data during the 12-minute periods before and after the down time. The dilution THA (column Q) is the corrected THA reading divided by the dilution ratio (from column Y). In column R we have the opportunity to compensate for the effect of moisture on the JUM detector. This was not done so column R equals column Q. Finally in column S, the hydrocarbon concentration is converted to a dry gas basis concentration.

In column T the hydrocarbon flow rate in g/min as carbon is calculated in a manner analogous to the water flow rate using the dry gas flow rate and the hydrocarbon concentration. Column U is the integral of column T over time, the cumulative hydrocarbon release up to that point in the schedule. Column V is the cumulative unit emissions, that is, column U divided by the oven-dry weight of the wood in the kiln.

Column X indicates the hydrocarbon sampling run and column Y is the dilution ratio during that run. The next two columns, Z and AA, are the cumulative dry gas and water during the kiln cycle. These are used obtain the average gas moisture contents. The corrected wood moisture content, as discussed in section VI, is shown in column AC. The kiln air and analyzer air moisture contents are shown in columns AD and AE.

At the end (bottom) of the FlowCalc spreadsheet are summaries by run of the flow data for the total hydrocarbon run intervals.

The other pages in the files "Hampton, Kiln.XLS" are graphs of the data in the FlowCalc page. Moisture content and board weight data are in the files named "Hampton, Board.XLS."

VI. Sampling Results

The hydrocarbon emissions are summarized graphically here. All emission data is presented in detail in Appendix 2.

Figure 4 shows total hydrocarbon concentration and vent rate versus time. The vent rate is high first 10 hours, and then decreases. The concentration increases to a peak of approximately 70 ppm as the kiln temperature is increased to 180°F over the first 15 hours. The concentration then decreases to a minimum at 25 to 30 hours. A slight increase occurs after this time as venting decreases. This is something we have often observed.

Figure 5 shows the cumulative hydrocarbon emissions and the rate of emissions versus time. The cumulative emissions (in grams) is the emissions up to any point in time in the schedule. One gram of emissions corresponds to 0.03 lb/mbf. The rate of emissions (in grams per minute) is how much is coming out per unit time. The maximum occurs at 15 to 20 hours after the temperature reaches its maximum and the drying rate is still high.

Figure 6 shows the wood moisture content versus time. The measured moisture content is obtained by doing a mass balance on the gas steams, then subtracting the water leaving the kiln from the initial moisture content of the wood. The estimated moisture content should most accurately represent the MC-time relationship because the initial and final moisture contents match the oven-dry test. This initial and final moisture contents were 70.7 and 16.1%, respectively.

Figure 7 shows the cumulative hydrocarbon emissions versus moisture content. The emissions for drying to any moisture content can be read from this graph. If, for example, a mill wanted to dry to 19% instead of 16.1%, the total hydrocarbon emissions could be estimated by adjusting the VOC level by 0.0038 lb/mbf/%MC (Table 3).

TABLE 3. Estimated VOC release at different final moisture contents.

Final	Diffe	VOC	
Moisture content	MC	VOC	release
%	%	lb/mbf	lb/mbf
12	4.1	0.016	0.253
13	3.1	0.012	0.249
14	2.1	0.008	0.245
15	0.1	0.004	0.241
16	0.1	0.000	0.237
16.1	0	0.000	0.237
17	-0.9	-0.003	0.234
18	-1.9	-0.007	0.230

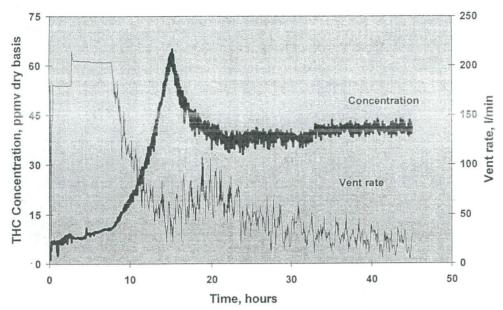


FIGURE 4. Hydrocarbon concentration and vent rate versus time.

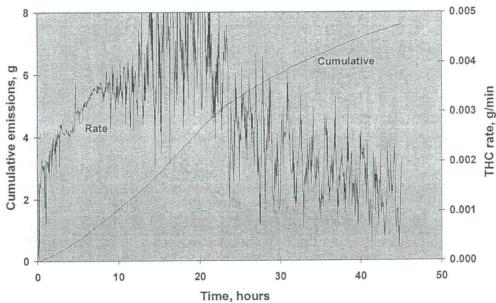


FIGURE 5. Cumulative emissions and rate of emissions versus time.

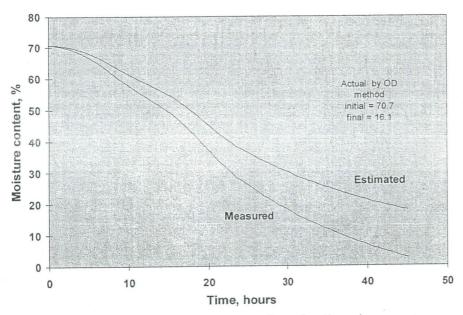


FIGURE 6. Moisture content versus time for the charge.

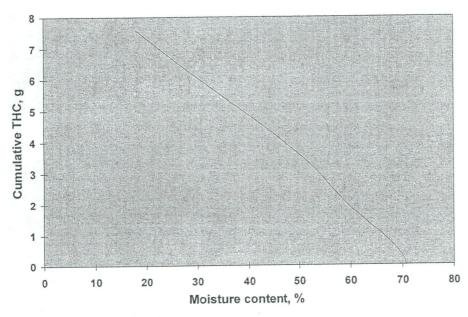


FIGURE 7. Cumulative emissions versus moisture content of the charge. One g is approximately 0.03 lbs.mbf.

Table 4 shows the VOC results by run for the charges. The interval time periods shown in the table include the times between sampling and mass calculations are adjusted to account for these. Sampling occurred for 96% of the total drying time as it took 5 to 10 minutes to check and calibrate the analyzer and set up dilution between three-hour sampling periods. Copies of all field sampling sheets, including dilution system and heated component data, in Appendix 3.

TABLE 4. Summary of sample runs for charge.

Sample	Time	Dry Flow	Wet Flow	THC	THC mass	THC rate		Average	
Run	711110	Rate @68	Rate @68	wet conc	as C	as C	Wood MC	Air MC	Anal. MC
11011	hrs	I/min	I/min	ppmv	lbs/mbf	lb/hr/mbf	%	%	%
1	2.75	187.4	192.0	6.6	0.010	0.0036	70.4	2.4	2.4
2	1.75	220.0	229.7	7.5	0.008	0.0047	69.2	4.2	4.2
3	4.50	206.8	222.2	9.9	0.027	0.0060	65.8	6.9	4.0
4	7.95	77.8	93.7	30.8	0.057	0.0072	57.3	17.0	9.8
5	4.55	74.0	97.5	31.0	0.038	0.0082	46.7	24.1	14.0
6	3.30	57.6	75.7	28.1	0.019	0.0058	38.9	24.0	13.9
7	3.75	46.1	60.6	29.1	0.018	0.0048	33.9	24.0	14.2
8	4.30	36.9	48.5	29.0	0.016	0.0038	31.4	23.9	13.9
9	8.25	29.0	38.2	30.7	0.027	0.0032	23.6	24.0	13.9
10	3.15	22.9	30.1	30.6	0.008	0.0025	23.1	23.9	14.1
11	4.55	16.7	21.9	31.4	0.009	0.0019	17.2	24.0	13.9
Sum	48.82				0.237				
Ave.		88.6	100.9	24.1		0.0047		18.0	10.8

VII Quality Assurance

Leak checks

Leak checks were performed on the VOC system before and after drying.

Calibration

Data for the calibration gases are given in Appendix 4. The mid gas was not named because the analyzer was within tolerance without naming. The calibration sheet for the flow meter is also included is also included in Appendix 4 as is the thermocouple calibration check.

VIII Discussion

There were no anomalies during the charges or unexpected problems that would affect the data.

Appendix 1. Detailed Sampling Procedures

INSTRUCTIONS FOR CHECKS OF EMISSIONS KILN

Purpose: Ensure kiln is operating correctly

Clock time: Record from computer

Run time: Record from computer. Check the box if the computer screen being refreshed and time is advancing.

Box temperature: Read from metal electrical box under desk, left controller. The top and bottom numbers should be similar on the box should be similar, about 126 C..

Valve temperature: Read from metal electrical box under desk, right controller. The top and bottom numbers should be similar on the box should be similar, about 154 C..

Dry-bulb temperature: Read from computer screen. Compare to graph to be sure it's correct. If it's not within a degree or two of the chart, check again in a few minutes. During startup (the first 3 or so hours), it may not be able to track. If it's too high, the heat valve should be closed, too low and the heat valve should be open. If it does not appear to be working correctly, call Mike or Mark.

Wet-bulb temperature: Read from computer screen. Compare to graph to be sure it's correct.

If it is too low, it means that the kiln atmosphere is too dry. Check the flow meters. If Flow1 is about 10 L/min (its lower limit), make sure that Flow2 and Flow3 are turned off

If it's too high, then either the kiln atmosphere is too humid or the sock is not being wetted. If Flow 1 is near 200 L/min (its upper limit) add venting by opening Flow2 and/or Flow 3. The maximum for Flow2 is 50 L/min, if it reads over this value for several readings, reduce it to about 45 L/min. Don't change Flow3 often, rather set it and leave it for several hours if possible. Keep the Flow 3 reading constant by small adjustments. As Flow1 decreases or Flow2 turned down, there is more pressure behind Flow3 and the flow increased. Check for water in the wet-bulb reservoir (push the float down and make sure it's getting water).

Check both Wet-bulb1 and Wet-bulb2 and make sure they are reading about the same. If they differ by more than 2 C, call Mike or Mark.

If both wet-bulbs are reading the same as the dry-bulb, check the wet-bulb water. If these procedures do not correct the wet-bulb temperature within 30 minutes, call Mike or Mark.

Line temperature: Read from gray box on wall above analyzer. It should read about 275°F.

Analyzer temperature: Push the temperature button on the analyzer. It should be in the 160 to 190°C range. When the lab is hot, it will read lower. Analyzer should usually be on range setting 3. All lights on the front of the analyzer should be green. The pressure should read about 200. Does the reading make sense - is it the same before and after an analyzer check; does increasing dilution cause a lower reading?

Chiller temperature: Read the chiller temperature. It should be about -1°C.

Flow 1: Read from computer. The value of Flow1 changes depending on the wet-bulb. If Flow 1 is 10 L/min and the wet-bulb is too low, there's probably nothing we can do. If it's 200 L/min and the wet-bulb is too high, Flow2 and/or Flow3 can be opened. Flow2 and Flow3 should be adjusted so that Flow1 stays below 175 to 200 L/min.

Dilution flow: Read dilution flow meter. It should read the same setting as the red flag. Do not adjust. If significantly different, investigate.

F/M Flow: Read from rotometer. This should be about 400 to 500 cc/min.

Line vacuum: Read from the vacuum gauge. This should be about 20"Hg.

INSTRUCTIONS - FIELD DATA SHEET FOR TOTAL HYDROCARBON ANALYZER PRE-SAMPLE PROCEDURE

BACKGROUND INFORMATION

Get the dry- and wet-bulb temperatures from the kiln schedule or off the computer. Use the highest expected values for the run.

Read absolute humidity off the psychrometric chart. Calculate

Percent moisture = 100 / [1 + 1 / 1.61*AbHum]
Target Dilution Ratio (TDR) = 15 / Percent Moisture

Event = the name of the drying cycle.

Run = the number of the 3-hour interval.

Operator, that's you.

Date and time are now, as you start the data collection process.

AMBIENT DATA

Call 9-754-0081 and get temperature and altimeter setting. Local pressure in Pascals = (Altimeter - 0.23) x 3.3867 Read the laboratory temperature from the thermometer.

ANALYZER CALIBRATION

Set valves so that 1, 2 = off; 3=on; 4=vent. This allows gas to flow out of the vents from the calibration tanks and shuts off all other sources. Only calibration gas should go through the detector.

Open the zero gas tank valve

zero toggle switch up (on), others down (off) set flow to 3.5 L/min using regulator on tank wait for a stable reading (about 30 to 60 seconds) use the zero dial (pot) on THA to get a zero reading read the analyzer read computer note pot setting close valve on zero gas tank

Open span gas tank valve

span toggle switch up (on), others down (off) set flow to 3.5 L/min using regulator on tank set analyzer to range 4 wait for a stable reading (about 30 to 60 seconds) use the span dial (pot) on THA to get a reading of 1527 ppm read the analyzer, record, for example, 1.53 as 1530 read computer (should read about 153 due to range 4 setting) note pot setting

Open mid gas tank valve

mid toggle switch up (on), others down (off) set flow to 3.5 L/min using regulator on tank set analyzer to range 3 wait for a stable reading (about 30 to 60 seconds) read analyzer (do not adjust pot settings), record, for example, 8.50 as 850 read computer (should about 850 with analyzer on range 3) check for within tolerance turn off mid gas all toggle switches off

SET DILUTION FLOW BEFORE RUN

Set valves so that 1, 2, 3 = off; 4=meter. This allows gas to flow only from the meter to the detector.

Use the Gilibrator to take 5 readings of the total flow rate (TFR). This is the total flow drawn by the analyzer and should be about 2.6 L/min

Make sure the average does not include any "bad" readings

Record the average, L/min = cc/min / 1000

Write the Event, Run, and "Pre-TFR" on the Gilibrator printout.

Calculate the next two values -

Target dilution flow rate (TDFR) is the TFR x (1 - DR)
Target sample flow rate (TSFR) is the TFR x DR
Check that the sum of these is the Total Flow Rate

Set dilution flow

Set red pointer to desired dilution flow (on meter with valve 1) Slowly open lower valve on dilution flow meter (1=on; 2, 3=off; 4=meter) Use upper valve on dilution flow meter to adjust flow Do not adjust this meter after this point Read the meter that you just set and record the value

Use the Gilobrator to take 5 readings of the sample flow rate (SFR). This is the flow through the analyzer after dilution is set. It will vary, depending on the dilution setting.

Make sure the average does not include any "bad" readings

Record the average, L/min = cc/min / 1000

Write "Pre-SFR" on the Gilobrator printout.

CHECK DILUTION FLOW BEFORE RUN

Set valves so that 1, 3 = on; 2=off; 4=vent. This allows gas to flow out of the vent from the calibration tank and shuts off all other sources. Calibration gas and dilution air will go through the detector.

Open span gas tank valve

span toggle switch up (on), others down (off) set flow to 3.5 L/min using regulator on tank wait for a stable reading (about 30 to 60 seconds) if reading is >9.99, switch to range 4 record set analyzer to range 3 turn off all calibration gas tank valves all toggle switches off

Calculate the dilution ratio based on gas flow by dividing the Sample Flow Rate by the Total Flow Rate.

Calculate the dilution ratio based on span gas by dividing the Diluted span by the undiluted span.

If the Dilution ratios do not agree within 5% - DO NOT PROCEED****. Use $100*(DR_{Span}$ - $DR_{Flow})/DR_{Flow}$ to calculate the % difference.

**** check calculations, check that values for ppm and flows make sense, remeasure everything. If it still does not agree, call Mike or Mark

START RUN

Set valve so that 1, 2, 5 = on; 3, 4=off; all calibration tank valves off Record the start time. Use the computer clock for all times or set your watch to the computer time. Make sure analyzer is on appropriate range, usually range 3, to keep THC reading on computer between 60 and 750.

Monitor system, as needed. Record system condition at least hourly. End time should be no more than 3 hours from start time.

POST-SAMPLE PROCEDURE

AT END OF RUN

Record your name as the operator.

Event = the drying cycle. Run = the 3-hour interval.

Operator, that's you. Date and time are now, as you start the data collection process.

AMBIENT DATA

Call 9-754-0081 and get temperature and altimeter

Local pressure = (Altimeter - 0.23) x 3.3867

Read the laboratory temperature from the thermometer.

Fill out appropriate information on Pre-sample side of data sheet for next run. This will save time in between runs.

END TIME

Record computer time.

DO NOT adjust dilution gas yet.

CHECK DILUTION FLOW AFTER RUN

Set valves so that 1, 3 = on; 2=off; 4=vent. This allows gas to flow out of the vent from the calibration tank and shuts off all other sources. Calibration gas and dilution air will go through the detector.

Open span gas tank valve

span toggle switch up (on), others down (off) set flow to 3.5 L/min using regulator on tank wait for a stable reading (about 30 -60 seconds) record all toggle switches off

Sample flow rate. Set valves so that 1=on; 2, 3 = off; 4=meter. This allows gas to flow only from the meter and the dilution to the detector.

Use the Gilibrator to take 5 readings of the sample flow rate (SFR). This is the flow through the analyzer with dilution on.

Make sure the average does not include any "bad" readings Record the average, L/min = cc/min / 1000

Write "Post-SFR" on the Gilibrator printout.

Read dilution flow meter To calculate the L/min, divide scfh by 2.12 Turn off dilution flow meter using valve 1

Total flow rate. Set valves so that 1, 2, 3 = off; 4=meter. This allows gas to flow only from the meter to the detector.

Use the Gilibrator to take 5 readings of the total flow rate (TFR). This is the total flow drawn by the analyzer and should be about 2.6 L/min Make sure the average does not include any "bad" readings Record the average, L/min = cc/min / 1000 Write "Post-TFR" on the Gilibrator printout.

CHECK CALIBRATION OF ANALYZER

Set valves so that 1, 2 = off; 3=on; 4=vent. This allows gas to flow out of the vents from the calibration tanks and shuts off all other sources. Only calibration gas should go through the detector.

Span gas tank valve should be open span toggle switch up (on), others down (off)

set flow to 3.5 L/min using regulator on tank set analyzer to range 4 wait for a stable reading (about 30 -60 seconds) read analyzer (do not adjust pot settings), record, for example, 1.50 as 1500 read computer (should read about 152 due to range 4 setting) note pot setting check for within tolerance - between 1483 and 1573

Open mid gas tank valve

mid toggle switch up (on), others down (off) set flow to 3.5 L/min using regulator on tank set analyzer to range 3 wait for a stable reading (about 30 -60 seconds) read analyzer (do not adjust pot settings), record, for example, 8.50 as 850 read computer (should read same as analyzer) check for within tolerance

Open the zero gas tank valve

zero toggle switch up (on), others down (off) set flow to 3.5 L/min using regulator on tank wait for a stable reading (about 30 -60 seconds) read analyzer (do not adjust pot settings) read computer note pot setting

Calculate the dilution ratio based on gas flow by dividing the Sample Flow Rate by the Total Flow Rate.

Calculate the dilution ratio based on gas flow by dividing the Sample Flow Rate by the Total Flow Rate.

Calculate % difference as 100 * {Absolute Value (DR_{Span}-DR_{Flow})} / DR_{Flow}

Record the time now as the end time for check.

Tear off the four sets of Gilibrator readings (Pre-TFR, Pre-SFR, Post-SFR, Post-TFR) and staple to paper with other records.

Start Pre-Sample procedure for next run.

Appendix 3. Samples of field data sheets.

Charge: Date:

Hampton 1

11-10-03

Board			Weights	
-5.11.0	Initial Wt.	Final Wt.	Oven	
	kg	kg	kg	
1- 1	2,165	1.40	1.290	
1- 2	2,405	1,690	1.465	
1- 3	2,290	1,485	11280	
1- 4	2285	1,595	1.360	
1- 5	2,225	1,575	1,335	
1- 6	2.100	1,415	1,245	
1- 7	2,360	1,475	1.270	
1- 8	2.250	1,430	1,230	
1- 9	2339	1,515	1,325	
1- 10	2,290	1,380	1,195	
1- 11	2,265	1,650	1,400	
1- 12	2.195	1,470	1,295	
1- 13	2,285	1.585	1370	pitch
1- 14	2070	1,415	1,220	V
1- 15	2120	1,485	1.200	
1- 16	5'590	1,570	,335	
1- 17	2,420	1,705	1.425	- A
1- 18	2,310	1,630	1,385	
1- 19	2,225	1.460	11265	
1- 20	2,275	1,400	1,205	
1- 21	2,40	1,640	1,40	
1- 22	2,290	1,530	1.330	
1- 23	2110	1,485	1,315	•
1- 24	2.065	1,410	1,235	
1- 25	2.395	1.605	1.355	
1- 26	2410	1,440	1.190	
1- 27	3,330	1,615	1.385	
1- 28	2,295	1,645	1,390	
	2345	1.655	1420	
1- 30	2,160	1.385	1.230	,

Sums: Averages: 0.000

0.000

0.000

			-	Line	inHa					B a dispas Dispassing principal principal												
				F/M	ml/min	-	1	1			\											
				Dilution	SCFM	Attention of the statement of the statem	1,5	1,5	I'S	1.5	1.5	1.5	5	5.7	15	1.5	7.	5	2,	1.5	INCOME. IN SECURITION OF SECUR	PARTO BIRE STREET ON BRIDE STREET
				2	in the second second							L										
				Flow 1	L/min	1	183	C81	20	126	96	07	7	54	53	∞	4	88	38	M3		
				Chiller	ာ့		goppingo	1)	1	~		\ \ -	\	_							
				Anlz	ပွ	180	192	192	66	192	193	192	193	193	107	192	192	193	193	981		
				Line	٦°	272	22	202	272	272	222	272	277	772	Da.	272	1271	272	222	777		
			es	2				7		7												
Time	(2:30	1:35	Temperatures	✓ Wet-bulb	၁့	100	32	42	99	R	49	53	59	79	99	59	99	79	79	53		
			1	-				9	- 1	1												
Date	80-01-11	11-12-03		Dry-bulb	၁့	0	35	23	74	100	78	80	8)	88	83	82	83	83	82	CB		
	0)-11	11-13		Valve	၁	135	75	145	ShI	145	15	145	145	53/1	145	元	12	148	145	16		
	Start:	End:		Вох	၁့	125	125	35	125	124	125	125	125	125	125	125	125	125	125	135		
			Run		#	一		3%	4	5	5	2	5	,	7	~	20		01	0		
				1	+	\dashv	+	- 1	7	7	-1	-	~ /	,	-	00	∞	0			-	\dashv
-	Hampton Affiliates		Run	time	hrs	0	7,50	6	16:53	17:11	14:08	£500t	21:32	3440	26,32	5,15 28:42	32.42	4206	4133 "	カボカ		
Charge:	натртог	Page:	Clock	time		12:33	3:15	THE REAL PROPERTY.		5,43	ンチ	8,25	45:6	18118	14:54	15/15	21:15	-		8:46 1		
								T. E. Charge and Street	11-11-03									12-03				

BACKGRO	OUND INFORMA	ATION					
Dry-bulb te	emperature:	0-165	Event (kiln charge): <u>Hampton 1</u>				
Wet-bulb te	emperature:	0-150	Run (sample):				
Absolute h	umidity:		Operator: MI	_			
	oisture:		Date: Nov	-	**************************************		
Target Dilu	tion Ratio (TDR):], ()	Time now :/		25		
AMBIENT	DATA						
Altimeter se	etting: <u>30,1</u>	9 inHg	Laboratory temp	oera	ture: 21 °C		
ANALYZER	R CALIBRATIO	V	ī	1. 2	= off; 3=on; 4=vent		
der i gelege e	Analyzer, ppm	Computer	Within range		Pot settings		
zero	(0)	NA	does not apply	y	395		
span	1 52 (1527)	NA	does not apply	У	381		
mid	8.76	NA	804 - 957		none		
		9					
	ION FLOW BE						
Total flow ra	ate (TFR):	1,725	_ L/min	[1	, 2, 3 = off; 4=meter]		
Target diluti	on flow rate (TD	FR)]	_L/min		[TFR x (1 - DR)]		
samp	ole flow rate (TS	FR)	_ L/min		[TFR×DR]		
Set and rea	d dilution meter:		scfh]	scfh = L/min * 2.12]		
Sample flow	v rate (SFR):		_ L/min [1 =	on;	2, 3 = off; 4=meter]		
CHECK DIL	UTION FLOW	BEFORE RUN		1.	3=on; 2=off; 4=vent]		
1	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR _{Flow} [SFR/TFR] 1	00*(Difference, % DR _{Span} - DR _{Flow})/DR _{Flow}		
Span	d			-			
START TIM	IE: 12137	T 4	2 5 = on: 3 4	= 0	iff: tank valves off 1		

[60 < computer reading < 750]

ANALYZER RANGE: 3

Operator: MRM		Event (kiln	charge): <u>Hampton 1</u>
Time now: 3:15 p		Run (sampl	e):
AMBIENT DATA			
Airport pressure:	_inHg	Laboratory temper	ature: 7/ °C
		-	
END TIME: 375	-		
CHECK DILUTION FLOW	FTER RUN	[1	, 3=on; 2=off; 4=vent]
	Analyzer		Computer
Span _{Diluted}	150		60
Sample flow rate (SFR) :	1	L/min [1= o	n, 2, 3 = off, 4=meter]
Read dilution meter:	scfh	_ L/min	[L/min = scfh*0.472]
Total flow rate (TFR): (attach print out with all four	sets of data	_L/min [1, 2, 3 = off; 4=meter]
Dilution ratio (DR _{Flow}):		_	[SFR/TFR]
CHECK OF ANALYZER CA	LIBRATION	[1	2=off; 3=on, 4=vent]
Analyzer	Computer	Within range	Pot settings
span 150	160	1481 to 1573	381
mid 817	921	804 to 957	none
zero	0	-45 to +45	395
Dilution ratio (DR _{Span}):	Management		[Span _{Diluted} / Span]
Dilution ratio difference:	### Charles Common Comm	% [100*(Abs(DR	Span - DR Flow))/DR Flow]
End time for check:	3120		
Comments: Leak C	hech 19.5	"-> 19,5"	over 3M/N
Are run	5		

BACKGR	OUND INFORMA	TION				
Dry-bulb t	emperature:	165F	Event (kiln charge): Hampton 1			
	temperature:<		Run (sample):	2		
Absolute I	humidity:		Operator: Mf			
Percent m	noisture:		Date:	-03		
Target Dil	ution Ratio (TDR)):	Time now :			
AMBIENT	DATA					
Altimeter		inHg	Laboratory tempera	ature:°C		
ANALYZE	R CALIBRATION	V	[1.3	2 = off: 3=on: 4=vent 1		
	Analyzer, ppm	Computer	Within range	Pot settings		
zero	(0)	O	does not apply	395		
span	15)(1527)	163	does not apply	:385		
mid	8 80	936	804 - 957	none		
SET DILU	TION FLOW BEI	ORE RUN				
Total flow	rate (TFR):	1726	_ L/min [1	, 2, 3 = off; 4=meter]		
Target dilu	ition flow rate (TD	FR)	L/min	[TFR x (1 - DR)]		
	nple flow rate (TS		L/min	[TFR x DR]		
Set and re	ad dilution meter	:	scfh	[scfh = L/min * 2.12]		
Sample flo	ow rate (SFR):		_ _ L/min	2, 3 = off; 4=meter]		
CHECK D	ILUTION FLOW	BEFORE RUN	[1,	3=on; 2=off; 4=vent]		
	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR Flow	Difference, % (DR _{Span} - DR _{Flow})/DR _{Flow}		
Span	ited			~		
	15.011					

START TIME: 15:24

[1, 2, 5 = on; 3, 4 = off; tank valves off]

ANALYZER RANGE: 2

[60 < computer reading < 750]

FIE	LD DATA SHEE	T FOR TOTAL HY	DROCAF	RBON ANAI	LYZER - POST
	MRM				charge): <u>Hampton 1</u>
Time now:	4:59				e): 2
			,	turi (sumpi	-)
AMBIENT	DATA				
Airport pre	ssure: <u>30,</u> 20	inHg	Laborat	tory tempera	ature:°C
END TIME	: 5:00				
		-			
CHECK DI	LUTION FLOW	1.0		[1,	3=on; 2=off; 4=vent
		Analyzer			Computer
L S	pan _{Diluted}	152			161
Sample flo	w rate (SFR) :	-	_ L/min	[1= or	n, 2, 3 = off, 4=meter]
Read diluti	on meter:	scfh	_ L/min		[L/min = scfh*0.472]
Total flow (attach prin	rate (TFR): nt out with all fou	r sets of data)	_ L/min	[1	, 2, 3 = off; 4=meter]
Dilution rat	io (DR _{Flow}):				[SFR/TFR]
CHECK OF	ANALYZER C	ALIBRATION		[1,	2=off; 3=on, 4=vent]
	Analyzer	Computer	Withi	in range	Pot settings
span	1,52	161	1481	to 1573	
mid	8,77	9.33	804	to 957	none
zero	0,01)		-45	to +45	
Dilution rat	io (DR _{Span}):				[Span _{Diluted} / Span]
Dilution rat	io difference:		% [10	0*(Abs(DR s	Span - DR Flow))/DR Flow]
End time fo	r check:	5:10			
Comments:					

Dry-bulb temperature: <82 C

Wet-bulb temperature: < 65C

Absolute humidity: < 0,2

Percent moisture: 25

Target Dilution Ratio (TDR): ___O.6__

Event (kiln charge): Hampton 1

Run (sample): ____

Operator: MRM

Date: Nov 10 03

Time now: 9:30p (21:30)

AMBIENT DATA

Altimeter setting:

30,20 inHg

Laboratory temperature: _____ °C

ANALYZER CALIBRATION [1				[1, 2	2 = off; 3=on; 4=vent]
	Analyzer, ppm		Computer	Within range	Pot settings
zero	0	(0)	0	does not apply	395
span	152	(1527)	9783 162	does not apply	385
mid	880		933	804 - 957	none

SET DILUTION FLOW BEFORE RUN

Total flow rate (TFR):

1,725 L/min

[1, 2, 3 = off; 4=meter]

Target

dilution flow rate (TDFR)

_____L/min

[TFR x (1 - DR)]

[TFR x DR]

sample flow rate (TSFR)

____L/min

[scfh = L/min * 2.12]

Sample flow rate (SFR):

Set and read dilution meter:

0,997 L/min

[1 = on; 2, 3 = off; 4=meter]

CHECK DILUT	[1, 3=on; 2=off; 4=vent]			
	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR Flow [SFR/TFR]	Difference, % 100*(DR _{Span} - DR _{Flow})/DR _{Flow}
Span _{Diluted}	883	0,58	0,58	0

START TIME: 9:40

[1, 2, 5 = on; 3, 4 = off; tank valves off]

ANALYZER RANGE:

[60 < computer reading < 750]

Operator:	and the figure of the second s	Event (kiln charge): Hampton 1				
Time now:	5138		Run (sample):			
AMBIENT Airport pre	DATA ssure: 30 25	inHg	Laborat	tory tempera	nture:_22_ °C	
END TIME	5128	_				
CHECK DI	LUTION FLOW	AFTER RUN		[1.	3=on; 2=off; 4=vent]	
	raporter and parameters are supported as the second residence of the second residence of the second residence	Analyzer			Computer	
S	pan _{Diluted}	884		9	40	
Sample flo	w rate (SFR) :	1,008	_ L/min	[1= or	n, 2, 3 = off, 4=meter]	
Read diluti	on meter: 1,5	scfh0,71	_ L/min		[L/min = scfh*0.472]	
Total flow r	rate (TFR): nt out with all fou	r sets of data)	_ L/min	[1	, 2, 3 = off; 4=meter]	
Dilution rat		0.57			[SFR/TFR]	
CHECK OF	ANALYZER CA	ALIBRATION		[1.	2=off; 3=on, 4=vent]	
	Analyzer	Computer	With	in range	Pot settings	
span	1,52	1628		to 1573	386	
mid	880	934	804	to 957	none	
zero	0	1		to +45	395	
Dilution rat	io (DR _{Span}):	0,58			[Span _{Diluted} / Span]	
Dilution rat	io difference:	1.7	% [10	00*(Abs(DR	Span - DR Flow))/DR Flow]	
End time for	or check:	5:36				
Comments	:					
	ne park i Wenny wang manandapina awas an arawana mahada amah a majar manasa an araw					

BACKGROUND	INFORMATION

Dry-bulb temperature: < 65 F

Wet-bulb temperature: < 150 F

Absolute humidity: ______02

Percent moisture: 25

Target Dilution Ratio (TDR): ___O,6

Event (kiln charge): Hampton 1

Run (sample): ____3

Operator: MRM

Time now: 5:00

AMBIENT DATA

Altimeter setting:

30,20 inHg

Laboratory temperature: 2/ °C

ANALYZER CALIBRATION [1, 2 = off; 3 = on; 4 = vent]Analyzer, ppm Computer Within range Pot settings 0 zero (0)does not apply 395 152 (1527) 161 span does not apply 385 600 mid 933 804 - 957 none

SET DILUTION FLOW BEFORE RUN

Total flow rate (TFR):

1,730 L/min

[1, 2, 3 = off; 4=meter]

Target

dilution flow rate (TDFR)

0.61 L/min

[TFR x (1 - DR)]

0.6

sample flow rate (TSFR)

1,038 L/min

[TFR x DR]

Set and read dilution meter:

1.5 scfh

[scfh = L/min * 2.12]

Sample flow rate (SFR):

________L/mir

L/min [1 = on; 2, 3 = off; 4=meter]

CHECK DILUT	[1, 3=on; 2=off; 4=vent]			
	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR Flow [SFR/TFR]	Difference, % 100*(DR _{Span} - DR _{Flow})/DR _{Flow}
Span _{Diluted}	863	057	0.57	

START TIME: 5,07

[1, 2, 5 = on; 3, 4 = off; tank valves off]

ANALYZER RANGE:

[60 < computer reading < 750]

Operator:	MRM			Event (kiln c	harge): <u>Hampton 1</u>
Time now:	9:30		I	Run (sample	e):3
AMBIENT	>			de secondo con consequencia de la consequencia de l	
Airport pre	ssure: <u>3020</u>	_ inHg	Labora	tory tempera	ature:°C
END TIME	: 9:31	-			
CHECK DI	LUTION FLOW	AFTER RUN		[1.	3=on; 2=off; 4=vent]
		Analyzer			Computer
S	pan _{Diluted}	887		942	
Sample flo	w rate (SFR) :	987			n, 2, 3 = off, 4=meter]
Read diluti	on meter: 15	scfh	L/min		[L/min = scfh*0.472]
Total flow r (attach prin	rate (TFR): nt out with all four				, 2, 3 = off; 4=meter]
Dilution rat		057			[SFR/TFR]
CHECK OF	ANALYZER CA	LIBRATION		ſ 1.	2=off; 3=on, 4=vent]
	Analyzer	Computer	With	in range	Pot settings
span	152	162		to 1573	385
mid	880	933	804	to 957	none
zero	0	0	-45	to +45	395
Dilution rat	io (DR _{Span}):	0,58			[Span _{Diluted} / Span]
Dilution rat	io difference:	<2	% [10	00*(Abs(DR	Span - DR Flow))/DR Flow]
End time fo	or check:	937			
Comments:	:	V			
	7				
ta de met fire de la respectación de la respectació	akt generalisen des frança tendes e generalisens en proprieta protesta arrano en mentre e en mentre arradismo				
audidus monte d'écologicament promission					

BACKGF	ROUND INFORMA	ATION	IDROCAR	BUN ANA	LYZER - PRE
Dry-bulb temperature: 82c Wet-bulb temperature: 65 c			Event (kiln charge): <u>Hampton 1</u> Run (sample):5		
Absolute	humidity:O	, 2		MI	
Percent n	noisture:	25	Date:	11-	11-03
Target Di	lution Ratio (TDR): _0.6	Time now	1:5	30
AMBIENT	DATA				
Altimeter	setting: 30 ,	25 inHg	Laborator	y tempera	ture: 22 °C
ANALYZ	R CALIBRATIO	V	, % r.	[1, 2	= off; 3=on; 4=vent
	Analyzer, ppm	Computer	Within		Pot settings
zero	(0)	0	does no	t apply	395
span	1530 (1527)	165	does no	t apply	389
mid	881	932	804 -	957	none
SET DILU	TION FLOW BEF	ORE RUN			3
Total flow	rate (TFR):	1,745	_L/min	[1	2, 3 = off; 4=meter]
Target dilu	tion flow rate (TD	FR)	_ L/min		[TFR x (1 - DR)]
san	nple flow rate (TS	FR)	_L/min		[TFR x DR]
Set and re	ad dilution meter:		_scfh]	scfh = L/min * 2.12]
Sample flo	w rate (SFR):	1,002	_L/min	[1 = on;	2, 3 = off; 4=meter]

(CHECK DILUT	[1, 3=on; 2=off; 4=vent			
-		Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR _{Flow} [SFR/TFR]	
	Span _{Diluted}	888	0,57	0,58	1,7%

START TIME: 5:40a

[1, 2, 5 = on; 3, 4 = off; tank valves off]

ANALYZER RANGE:

[60 < computer reading < 750]

Operator:	erator: MRM Event (kiln charge): Hampto				harge): <u>Hampton 1</u>	
Time now:	9:50		Run (sample):5			
AMBIENT	DATA		antigen de contracte por Arango de paracet como secondo	in the contract of the contrac		
Airport pre	ssure: <u>30, 34</u>	inHg	Laborat	tory tempera	ature: 21 °C	
END TIME	: 9:57	_				
CHECK DI	LUTION FLOW	AFTER RUN		[1.	3=on; 2=off; 4=vent]	
		Analyzer		-	Computer	
S	Span _{Diluted}	882		93		
Sample flo	w rate (SFR) :	1,001	_ L/min	[1= or	n, 2, 3 = off, 4=meter]	
Read diluti	on meter: <u>1,5</u>	scfh	_ L/min		[L/min = scfh*0.472]	
Total flow r	rate (TFR): nt out with all fou	r sets of data)	_ L/min	[1	, 2, 3 = off; 4=meter]	
	tio (DR _{Flow}):	0.58			[SFR/TFR]	
CHECK O	F ANALYZER C	ALIBRATION		[1.	2=off; 3=on, 4=vent 1	
	Analyzer	Computer	With	in range	Pot settings	
span	1510	1630	1481	to 1573	398	
mid	875	931	804	to 957	none	
zero	0		-45	to +45	395	
Dilution rat	io (DR _{Span}):	0,58			[Span _{Diluted} / Span]	
Dilution rat	io difference:		% [10	0*(Abs(DR	Span - DR Flow))/DR Flow]	
End time fo	or check:	10:02				
Comments:						
p4-radylinestiquillusty, pudosene and orange missionals.						

BACKGROUND INFORM	ATION			
Dry-bulb temperature: Wet-bulb temperature: Absolute humidity: Percent moisture: Target Dilution Ratio (TDR)	65 0,2 25	Event (kiln charge): Hampton 1 Run (sample): 6 Operator: MRM Date: 11-11-03 Time now: 9:50		
AMBIENT DATA				
Altimeter setting: 30	:34 inHg	Laboratory tempe	rature:2/°C	
ANALYZER CALIBRATIO	N	· · · · · · · · · · · · · · · · · · ·	2 = off; 3=on; 4=vent]	
Analyzer, ppm	Computer	Within range	Pot settings	
zero (0)		does not apply	392	
span /52 (1527)	1647	does not apply	395	
mid 88)	935	804 - 957	none	
SET DILUTION FLOW BEI	ORE RUN			
Total flow rate (TFR):	1,731	_L/min [1, 2, 3 = off; 4=meter]	
Target dilution flow rate (TD	FR)	_L/min	[TFR x (1 - DR)]	
sample flow rate (TS	FR)	_ L/min	[TFR x DR]	
Set and read dilution meter	1,5	_scfh	[scfh = L/min * 2.12]	
Sample flow rate (SFR):	1,004	_L/min [1 = on	; 2, 3 = off; 4=meter]	
CHECK DILUTION FLOW	BEFORE RUN	[1	3=on; 2=off; 4=vent]	
Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR _{Flow} [SFR/TFR] 100	Difference, % *(DR _{Span} - DR _{Flow})/DR _{Flow}	
Span _{Diluted} 953	0,580	0,59	2	

START TIME: 10:07

[1, 2, 5 = on; 3, 4 = off; tank valves off]

ANALYZER RANGE:

[60 < computer reading < 750]

Operator: MRM				Event (kiln charge): Hampton 1		
Time now:	1:15		Run (sample):			
AMBIENT	DATA					
Airport pre	ssure: <u>30,25</u>	_ inHg	Laborat	ory tempera	ature: <u> </u>	
END TIME	:1120	-				
CHECK DI	LUTION FLOW	AFTER RUN		[1,	3=on; 2=off; 4=vent]	
		Analyzer			Computer	
S	pan _{Diluted}	899		94	14	
Sample flo	w rate (SFR) :	1010	_L/min	[1= or	n, 2, 3 = off, 4=meter]	
Read diluti	on meter: 1,5	scfh	L/min		[L/min = scfh*0.472]	
Total flow r (attach prin	rate (TFR): nt out with all four	sets of data)	Z L/min	[1	, 2, 3 = off; 4=meter]	
Dilution rat		0,581			[SFR/TFR]	
CHECK OF	ANALYZER CA	LIBRATION		[1.	2=off; 3=on, 4=vent]	
	Analyzer	Computer	With	in range	Pot settings	
span	153	166	1481	to 1573		
mid	883	9'36	804	to 957	none	
zero	0	1	-45	to +45		
Dilution rat	io (DR _{Span}):	0,587			[Span _{Diluted} / Span]	
Dilution rat	io difference:	0/88/0	% [10	0*(Abs(DR	Span - DR Flow))/DR Flow]	
End time fo	or check:	1:25				
Comments:		3				
del anni diversio si ampi dina rusha assaula assaula						

BACKGR	ROUND INFORM	ATION			
Dry-bulb temperature:			Event (kiln charge): Hampton 1 Run (sample): Operator:MRM Date:/I-/I-03 Time now:lis		
AMBIENT					- 14.8
Altimeter	setting: 30	inHg	Laboratory ten	nperati	ure:_2 °C
ANALYZE	R CALIBRATIO	Y		[1,2:	= off; 3=on; 4=vent]
	Analyzer, ppm	Computer	Within rang	е	Pot settings
zero	(0)	1.	does not app	oly	392
span	1530) (1527)	166	does not app	oly	392
mid	883	936	804 - 957		none
Total flow	TION FLOW BEI	FORE RUN	no dilution L/min	[1, :	2, 3 = off; 4=meter]
Target dilu	tion flow rate (TD	FR)	L/min		[TFR x (1 - DR)]
san	nple flow rate (TS	FR)	L/min		[TFR x DR]
Set and re	ad dilution meter		scfh	ſs	scfh = L/min * 2.12]
Sample flo	w rate (SFR):	1,008.	0/hr/12h L/min [1 =		2, 3 = off; 4=meter]
CHECK D	ILUTION FLOW	BEFORE RUN		ſ 1. 3:	on: 2=off: 4=vent 1
	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR _{Flow} [SFR/TFR]		Difference, % R _{Span} - DR _{Flow})/DR _{Flow}
Span _{Dilut}	ted 887	958	0,58		0
START TI	we: 1:24	T 4	2 E = op: 2	A = 05	f. tamle value a ser

[60 < computer reading < 750]

ANALYZER RANGE: _

Operator:	MRM	and the second second speciments.	Event (kiln o	charge): <u>Hampton 1</u>
Time now:	5:07		Run (sample	e):
AMBIENT Airport pre	DATA ssure: 30,24	<u></u> inHg	Laboratory temper	ature:°C
END TIME	: 5,07			
CHECK DI	LUTION FLOW	AFTER RUN Analyzer	-	3=on; 2=off; 4=vent] Computer
S	pan _{Dilluted}	88)	0	141
Sample flo	w rate (SFR) :	1.004		n, 2, 3 = off, 4=meter]
Read diluti	on meter: <u>15</u>	scfh	Desire Control of the	[L/min = scfh*0.472]
Total flow reaction (attach prin	rate (TFR): nt out with all fou	r sets of data)	L/min [1, 2, 3 = off; 4=meter]
	io (DR _{Flow}):	058		[SFR/TFR]
CHECK O	ANALYZER C	ALIBRATION	[1	2=off; 3=on, 4=vent]
	Analyzer	Computer	Within range	Pot settings
span	1530	1620	1481 to 1573	395
mid	884	940	804 to 957	none
zero	0	1	-45 to +45	395
Dilution rat	io (DR _{Span}):	0,58	5 × 7	[Span _{Diluted} / Span]
Dilution rat	io difference:	O	% [100*(Abs(DR	Span - DR Flow))/DR Flow]
End time fo	or check:	5:10		
Comments	:			
		and and the second are the second are second and the second and the second are second as a second as a second		
	akkaan maanaha kaan katan kaan kaan kaan kaan kaan ka			
-				

BACKGR	OUND INFORMA	ATION		
Dry-bulb t Wet-bulb Absolute t Percent m	temperature: temperature: temperature: humidity: noisture: ution Ratio (TDR	65 0,2 25): 0,6	Event (kiln charge Run (sample):	8 RM -11-03
Altimeter	setting: 30	124 inHg	Laboratory temper	ature:°C
ANALYZE	R CALIBRATIO	V		2 = off; 3=on; 4=vent 1
	Analyzer, ppm	Computer	Within range	Pot settings
zero	Z (0)		does not apply	7
span	5克曼 (1527)	0	does not apply	
mid	Sos S		804 - 957	none
SET DILU	TION FLOW BER	ORE RUN		
	rate (TFR):	1739	L/min [1	, 2, 3 = off; 4=meter]
Target dilut	tion flow rate (TD	FR)	L/min	[TFR x (1 - DR)]
sam	ple flow rate (TS	FR)	L/min	[TFR x DR]
Set and rea	ad dilution meter:	1.5	_ scfh	[scfh = L/min * 2.12]
Sample flor	w rate (SFR):	997	L/min [1 = on;	2, 3 = off; 4=meter]
CHECK DI	LUTION FLOW	BEFORE RUN	[1,	3=on; 2=off; 4=vent]
	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR Flow [SFR //TFR] 100*	Difference, % (DR _{Span} - DR _{Flow})/DR _{Flow}
Span	ed		10/59	
START TIM	ME: 5:13	_ [1	1, 2, 5 = on; 3, 4 = o	off; tank valves off]
ANALYZEF	R RANGE:	2	[60 < compi	iter reading < 750 1

[60 < computer reading < 750]

Operator: MRM		Е	vent (kiln cha	arge): <u>Hampton 1</u>
Operator: MRM Time now: 9715	pm	R	tun (sample):	9
AMBIENT DATA				
Airport pressure: 300	13_inHg	Laborate	ory temperatu	ıre:20_ °C
END TIME: 9120pv	n			
CHECK DILUTION FLO	WAFTER RUN		[1, 3=	on; 2=off; 4=vent]
	Analyzer		Co	omputer
Spanniluted	934		97	2
Sample flow rate (SFR)		_L/min	[1= on,	2, 3 = off, 4=meter]
Read dilution meter: 1	5 scfh	_ L/min	[L	/min = scfh*0.472]
Total flow rate (TFR): (attach print out with all	four sets of data)	_L/min	[1,2	2, 3 = off; 4=meter]
Dilution ratio (DR _{Flow}):	0,59	_		[SFR/TFR]
CHECK OF ANALYZER	CALIBRATION		[1,2=	off; 3=on, 4=vent]
Analyzer	Computer	Withi	n range	Pot settings
span 1,590		1481	to 1573	
mid 883	938	804	to 957	none
zero		-45	to +45	
Dilution ratio (DR _{Span}):	0.61		. 1	[Span _{Diluted} / Span]
Dilution ratio difference:		% [10	0*(Abs(DR _{Spal}	n - DR _{Flow}))/DR _{Flow}]
End time for check:				
Comments:				
FILL	- 103°c)	- Y	Was 19	00
THA Tem	m=180C, bi	1 M	has 1	1 + 10
monues à	when Thon	At C	and VAC	1 192
3 dhis was	probably affector	on		

BACKGROU	ND INFORM	ATION		÷	
	perature:		Event (kiln charge): Hampton 1		
Wet-bulb tem	perature:	65	Run (sample):		
Absolute hun	nidity:O,	16	Operator:	MR	M
Percent mois	ture:	4	Date://	1-11-	03
Target Dilution Ratio (TDR):		Time now :		7:15p	
AMBIENT DA	ATA				
Altimeter setti	ing: $30,0$	<u>43</u> inHg	Laboratory te	mpera	nture: ⊋ሪ°C
ANALYZER (CALIBRATIO	N		[1 2	= off; 3=on; 4=vent
Ar	nalyzer, ppm	Computer	Within rang		Pot settings
zero Z	70 (O)		does not ap	ply	395
span	F 77 (1527)		does not ap	ply	398
mid	25		804 - 957		none
SET DILUTIO	N FLOW BE	ORE RUN			
Total flow rate		1.746	_L/min	[1	, 2, 3 = off; 4=meter]
Target dilution	flow rate (TD	FR)	_L/min		[TFR x (1 - DR)]
sample	flow rate (TS	FR)	_L/min		[TFR x DR]
Set and read o	dilution meter:	1.5	_scfh		scfh = L/min * 2.12]
Sample flow ra	ate (SFR):	1,013	_L/min [1		2, 3 = off; 4=meter]
CHECK DILU	ION FLOW	BEFORE RUN			3=on; 2=off; 4=vent 1
2	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR Flow [SFR/TFR]		Difference, % DR _{Span} - DR _{Flow})/DR _{Flow}
Span _{Diluted}	903	0,59	0.58		2
		,			

START TIME: 9:30 pm

[1, 2, 5 = on; 3, 4 = off; tank valves off]

ANALYZER RANGE: ____

[60 < computer reading < 750]

Operator:	•	or specific distribution of the specific of th	E	Event (kiln c	harge): <u>Hampton 1</u>
Time now:	5:36	responsação compressor de la compressão	F	Run (sample	e):
AMBIENT	DATA			interes aucadrescritice reservant proposant automobile de l'estant	
Airport pre	ssure: 3042	_ inHg	Laborat	ory tempera	ature: 7 °C
END TIME	: 5136	-			
CHECK DI	LUTION FLOW	AFTER RUN		<u> </u>	3=on; 2=off; 4=vent 1
		Analyzer		_	Computer
S	pan _{Diluted}	901		95	5
	w rate (SFR) :	1023		[1= or	n, 2, 3 = off, 4=meter]
Read diluti	on meter: <u> </u>	scfh	_ L/min		[L/min = scfh*0.472]
Total flow r (attach prin	rate (TFR): nt out with all four	sets of data)	_ L/min	[1	, 2, 3 = off; 4=meter]
Dilution rat		1884			[SFR/TFR]
CHECK OF	ANALYZER CA	LIBRATION		<u> </u>	2=off; 3=on, 4=vent]
	Analyzer	Computer	With	in range	Pot settings
span	1540	1647	1481	to 1573	395
mid	889	948	804	to 957	none
zero	0		-45	to +45	395
Dilution rat	io (DR _{Span}):	0,585			[Span _{Diluted} / Span]
Dilution rat	io difference:	0,3	% [10	0*(Abs(DR	Span - DR Flow))/DR Flow]
F 16 - 6		5:44			
End time for	or check:	3.74			
Comments					
		Microscopine agranda com manufacco con del matema que nos contratas por contrata de contrata de contrata de co			ti til det skallet i til til til til til til til til til
MACON CONTROL OF CONTR					

BACKGRO	UND INFORMA	ATION			
Dry-bulb te	mperature:	82	Event (kiln ch	arge):	: Hampton 1
Wet-bulb te	emperature:	5	Run (sample):/ 0		
Absolute humidity:		Operator:			
Percent moisture: 25		Date://~/		_	
Target Dilu	tion Ratio (TDR):	Time now :	5:1	+2
AMBIENT I	DATA			8	
Altimeter se	etting: <u>30</u>	142 inHg	Laboratory ter	npera	ture: 19 °C
ANALYZEF	R CALIBRATIO	V		[1.2	= off; 3=on; 4=vent]
	Analyzer, ppm	Computer	Within rang	1	Pot settings
zero	(0)	1	does not app	oly	392
span	1520 (1527)	1638	does not app	oly	390
mid	883	937	804 - 957		none
SET DILUT	ION FLOW BEF	ORE RUN			
Total flow ra	ate (TFR):	1.748	_L/min	[1,	2, 3 = off; 4=meter]
Target dilutio	on flow rate (TD	FR)	_ L/min		[TFR x (1 - DR)]
samp	le flow rate (TS	FR)	_ L/min		[TFR x DR]
Set and read	d dilution meter:	9,5	_scfh]	scfh = L/min * 2.12]
Sample flow	rate (SFR):	0,999	_ L/min [1 =	on;	2, 3 = off; 4=meter]
CHECK DIL	UTION FLOW	BEFORE RUN		[1, 3	3=on; 2=off; 4=vent]
	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR _{flow} [SFR/TFR]	100*([Difference, % DR _{Span} - DR _{Flow})/DR _{Flow}
SpanDiluted	892	0,586	0,572		1
START TIME	E: _5:47	_ [1	, 2, 5 = on; 3,	4 = of	ff; tank valves off]
NALYZER	NALYZER RANGE: [60 < computer reading < 750]				

CHECK OF ANALYZER CALIBRATION [1, 2=off; 3=on, 4=vent] Analyzer Computer Within range Pot settings span 1500 1611 1481 to 1573 \$972 mid 871 924 804 to 957 none zero 0 -45 to +45 392	Operator:	MKM	and appearing the sand of the	E	Event (kiln c	harge): <u>Hampton 1</u>
Airport pressure: 3039 inHg Laboratory temperature: 20 °C END TIME: 5:49 CHECK DILUTION FLOW AFTER RUN [1, 3=on; 2=off; 4=vent] Analyzer Computer Span_Diluted 890 946 Sample flow rate (SFR): 1,019 L/min [1= on, 2, 3 = off, 4=mete] Read dilution meter: 5 scfh L/min [L/min = scfh*0.472] Total flow rate (TFR): 1,749 L/min [1, 2, 3 = off; 4=mete] (attach print out with all four sets of data) Dilution ratio (DR _{Flow}): 0.58 [SFR / TFR] CHECK OF ANALYZER CALIBRATION [1, 2=off; 3=on, 4=vent] Analyzer Computer Within range Pot settings span 1500 1611 1481 to 1573 972 mid 87/ 924 804 to 957 none zero 0 145 to +45 392 Dilution ratio (DR _{Span}): 0.59 [Span_Diluted / Span] Dilution ratio difference: 1.7 % [100*(Abs(DR Span - DR Flow))/DR Flow] End time for check: 9:54	Time now:	8:47		F	Run (sample	e): <u>10</u>
CHECK DILUTION FLOW AFTER RUN Analyzer Span_Diluted Span S	AMBIENT	DATA	a coloradora e cisto e e e e e e e e e e e e e e e e e e e			
CHECK DILUTION FLOW AFTER RUN Analyzer Span _{Diluted} Span _{Diluted} Span _{Diluted} Span _{Diluted} Span _{Diluted} Span _{Diluted} Sample flow rate (SFR): L/min [1= on, 2, 3 = off, 4=meter L/min [1, 2, 3 = off, 4=meter L/min	Airport pre	essure: <u>30,39</u>	inHg	Laborat	ory tempera	ature: 20 °C
CHECK DILUTION FLOW AFTER RUN Analyzer Span_Diluted Spa						
Analyzer Computer Span_Diluted SPQ 9/6 Sample flow rate (SFR): 1,019 L/min [1= on, 2, 3 = off, 4=meter Read dilution meter: 1.5 scfh L/min [L/min = scfh*0.472] Total flow rate (TFR): 1,749 L/min [1, 2, 3 = off, 4=meter (attach print out with all four sets of data) Dilution ratio (DR _{Flow}): [SFR / TFR CHECK OF ANALYZER CALIBRATION [1, 2=off; 3=on, 4=vent Analyzer Computer Within range Pot settings span 1500 161 1481 to 1573 892 mid 87/ 924 804 to 957 none zero 0 1 4-75 to +45 392 Dilution ratio (DR _{Span}): [Span _{Diluted} / Span Dilution ratio difference: 1.7 % [100*(Abs(DR _{Span} - DR _{Flow}))/DR _{Flow} End time for check: 8:54	END TIME	: 8:48	- -			
Span _{Diluted} Sample flow rate (SFR):	CHECK D	ILUTION FLOW	AFTER RUN		[1,	3=on; 2=off; 4=vent
Sample flow rate (SFR):			Analyzer			Computer
Read dilution meter: $\frac{1}{1}$ scfh $\frac{1}{1}$ L/min $\frac{1}{1}$ [L/min = scfh*0.472] Total flow rate (TFR): $\frac{1}{1}$ L/min $\frac{1}{1}$ 1, 2, 3 = off; 4=meter (attach print out with all four sets of data) Dilution ratio (DR _{Flow}): $\frac{1}{1}$ Span $\frac{1}{1}$ 1, 2=off; 3=on, 4=vent $\frac{1}{1}$ 2=off; 3=on, 4=vent $\frac{1}{1}$ 3 span $\frac{1}{1}$ 1, 2=off; 3=on, 4=vent $\frac{1}{1}$ 2 within range $\frac{1}{1}$ Pot settings $\frac{1}{1}$ span $\frac{1}{1}$ 1, 2=off; 3=on, 4=vent $\frac{1}{1}$ 2 within range $\frac{1}{1}$ 2 settings $\frac{1}{1}$ 3 span		Span _{Diluted}	890			146
Total flow rate (TFR): (attach print out with all four sets of data) Dilution ratio (DR _{Flow}): [SFR / TFR CHECK OF ANALYZER CALIBRATION [1, 2=off; 3=on, 4=vent] Analyzer Computer Within range Pot settings span 1500 1611 1481 to 1573 992 mid 871 924 804 to 957 none zero 0 401 401 401 401 401 401 401 Dilution ratio (DR _{Span}): [Span _{Diluted} / Span Dilution ratio difference: 1,7 % [100*(Abs(DR _{Span} - DR _{Flow}))/DR _{Flow} End time for check: 9.54	Sample flo	w rate (SFR) :	1,019	_ L/min	[1= or	n, 2, 3 = off, 4=meter
Dilution ratio (DR _{Flow}): CHECK OF ANALYZER CALIBRATION Analyzer Computer Within range Pot settings span 1500 61 1481 to 1573 972 mid 871 724 804 to 957 none zero Dilution ratio (DR _{Span}): Dilution ratio difference: 17 % [1, 2=off; 3=on, 4=vent vent yes	Read dilut	ion meter: 15	scfh	_ L/min		[L/min = scfh*0.472
Dilution ratio (DR _{Flow}): CHECK OF ANALYZER CALIBRATION Analyzer Computer Within range Pot settings span 1500 61 1481 to 1573 972 mid 871 724 804 to 957 none zero Dilution ratio (DR _{Span}): Dilution ratio difference: 17 % [1, 2=off; 3=on, 4=vent vent yes	Total flow (attach pri	rate (TFR): nt out with all fou	r sets of data)	_ L/min	[1	, 2, 3 = off; 4=meter
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$				_		[SFR/TFR
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	CHECK O	F ANALYZER C	ALIBRATION		ſ 1.	2=off: 3=on, 4=vent
mid $87/$ 924 804 to 957 none zero 0 -45 to $+45$ 392 Dilution ratio (DR _{Span}): 059 [Span _{Diluted} / Span Dilution ratio difference: 17 % [$100*(Abs(DR_{Span} - DR_{Flow}))/DR_{Flow}$] End time for check: 9.54				With	-	
zero 0 -45 to +45 392 Dilution ratio (DR _{Span}): 059 [Span _{Diluted} / Span Dilution ratio difference: 17 % [100*(Abs(DR _{Span} - DR _{Flow}))/DR _{Flow} End time for check: 9.54	span	1500	1611	1481	to 1573	397
Dilution ratio (DR _{Span}): $0.5.9$ [Span _{Diluted} / Span Dilution ratio difference: 1.7 % [100*(Abs(DR _{Span} - DR _{Flow}))/DR _{Flow} End time for check: 9.54	mid	871	924	804	to 957	none
Dilution ratio difference: 1.7 % [$100*(Abs(DR_{Span} - DR_{Flow}))/DR_{Flow}$] End time for check: 9.54	zero	0		-45	to +45	392
End time for check: <u>\$.54</u>	Dilution ra	tio (DR _{Span}):	059			[Span _{Diluted} / Span
	Dilution ra	tio difference:	1.7	% [10	00*(Abs(DR	_{Span} - DR _{Flow}))/DR _{Flow}
Comments:	End time for	or check:	8:54			
	Comments	s:				
			achtun ann an ann an an an an an an an an an			

BACKGROL	JND INFORMA	ATION			
Wet-bulb temperature: 65 Absolute humidity: 0,16		Event (kiln charge): <u>Hampton 1</u> Run (sample):			
	sture:		Date: //	,	
Target Dilution Ratio (TDR):		Time now :			
AMBIENT DA	ATA			*8	
Altimeter set	ting: 30	39_inHg	Laboratory tem	npera	ture:_ <i>26</i> °C
ANALYZER	CALIBRATIO	N		[12	= off; 3=on; 4=vent]
	nalyzer, ppm	Computer	Within range	1	Pot settings
zero	(0)	/	does not app	ly	392
span	152 (1527)	1636	does not app	ly	392
mid	870	921	804 - 957		none
SET DILUTIO	ON FLOW BE	ORE RUN			
Total flow rate	e (TFR):	1,752	_L/min	[1,	2, 3 = off; 4=meter]
Target dilution	n flow rate (TD	FR)	_L/min		[TFR x (1 - DR)]
sample	e flow rate (TS	,	_L/min		[TFR x DR]
Set and read	dilution meter	1,5	_scfh	[scfh = L/min * 2.12]
Sample flow r	ate (SFR):	1,029	_ L/min	on;	2, 3 = off; 4=meter]
CHECK DILU	TION FLOW	BEFORE RUN		[1.3	3=on; 2=off; 4=vent]
	Analyzer	DR _{Span} [Span _{Diluted} /Span]	DR Flow [SFR/TFR]	100*(Difference, % DR _{Span} - DR _{Flow})/DR _{Flow}
Span _{Diluted}	910	0.59	0.59		
	0:00				

START TIME: 9:00

[1, 2, 5 = on; 3, 4 = off; tank valves off]

ANALYZER RANGE: 2

[60 < computer reading < 750]

	Operator: _	MRM	contribution and the contribution of the contr	E	Event (kiln c	charge): <u>Hampton 1</u>
	Time now:	15 5		F	Run (sample	e): 3
	AMBIENT I	DATA				
	Airport pres	ssure: <u>30,34</u>	inHg inHg	Laborat	ory tempera	ature: 20 °C
12:00	END TIME:	1:23				
	CHECK DIL	LUTION FLOW	AFTER RUN		[1,	3=on; 2=off; 4=vent
			Analyzer			Computer
	S	pan _{Diluted}	885		95	5 0
	Sample flov	v rate (SFR):	1005	_ L/min	[1= or	n, 2, 3 = off, 4=meter]
	Read dilution	on meter: <u>1,5</u>	scfh	_ L/min		[L/min = scfh*0.472]
	Total flow ra (attach prin	ate (TFR): t out with all fou	r sets of data)	<u></u> ∠/min	[1	1, 2, 3 = off; 4=meter]
	Dilution rati	o (DR _{Flow}):	0.580			[SFR/TFR]
	CHECK OF	ANALYZER C	ALIBRATION	·	[1,	2=off; 3=on, 4=vent]
		Analyzer	Computer	With	in range	Pot settings
	span	15/0	0	1481	to 1573	390
	mid	874	^	804	to 957	none
	zero	0	~	-45	to +45	3.92
	Dilution rati	o (DR _{Span}):	0.586			[Span _{Diluted} / Span]
	Dilution ration	o difference:		% [10	0*(Abs(DR	Span - DR Flow))/DR Flow]
	End time for	r check:	1:31			
	Comments:	Leak o	lech post	- [0	1.5 @1.	33:67
	19	"@ SAA	1981/0	1:42 pm	И	
	-			1	efriði er frætti ar særnu skalenskur lyknað er sjárlaði.	

Appendix 4. Calibration Data



BOC GASES VANCOUVER, WASHINGTON

: 13-MAY-2003 : 12-MAY-2008 : 25965 : 2200 psig : CGA-346 Approx. Pressure CGA Outlet **Expiration Date** Fill Date

Lot Number

Order Number

Air, Zero 0.1

Concentration

161 : 2 COMP MK BAL AIR
GYLINDER CONTENT ANALYSIS

Component

proparie

: 19-JUL-2003 : 19-JUL-2000

> Expired Material

E

CGA Outlet: 200/F90 BR 3360

: 2000 paig : 10805900

Pressure

#no

Cylinder# : 389264

BALANCE

881 ppm

CYLINDER CONTENT ANALYSIS
Omponent
Concentration < 3 ppm < 0.1 ppm 22.8 % Balance Total Hydrocarbon Component Nitrogen Moisture Oxygen

BOC GASES VANCOUVER, WASHINGTON

Sylinder Number CC85608

527 PPM 5/1/00 2000 152 590 Cyl. Pressure CGA Outlet Cyl. Size Fill Date Amount

Test # 99060814

PROPANE 1500 PPM AIR BALANCE





: 2200 psig : CGA350 : 07-FEB-2002 : 06-FEB-2007 : GS-1430 Approx. Pressure Order Number CGA Outlet

VAN-01-24798 Expiration Date Lot Number Fill Date

Hydrogen

CYLINDER CONTENT ANALYSIS
omponent Consentration 89.999% Component -lydrogen

0.43 ppm 0.05 ppm Carbon Dioxide Nitrogen Oxygen

<0.09 ppm <0.09 ppm 1.61 ppm <10.0 ppm + Carbon Monoxide Total Hydrocarbons Moisture Total Impurities

TC Calibration					
6/10/2002					
Omega	PC				
Calibrator	Readout				
С	C				
30.0	30.0				
50.0	50.1				
70.0	70.1				
90.0	90.1				
110.0	110.0				



Flow Calibration Record Sheet (200 SLM)

ERA#: 128989W

Customer: OREGON STATE UNIVERSITY

MKS Transfer Standard Type: 1559A-200L-SV

MKS Primary Standard Type: A-200-1

Serial Number: WS 136

Serial Number: 14952-1-1

Standard Flow Rate (SLM)	UUT Flow Rate (SLM)	UUT Error (SLM)	Percent of full scale Error
0.00	0.000	0.000	0.000%
50.000	50.880	0.880	0.440%
100.000	99.880	-0.120	-0.060%
150.000	150.040	0.040	0.020%
200.000	200.000	0.000	0.000%

UUT Model: 1559A-200L-SV

Process Gas used:

UUT Process Gas:

N2

Date of Calibration: 05/10/00

UUT Serial #: 000317785

UUT Range:

200 SLM

Calibrated by: DP

Verified by:

Notes:

- 1. All units must be operated on regulated heat (Power on) for a minimum of of one hour before any adjustment is made.
- 2. Flowmeters and/or Controllers are Calibrated at atmospheric pressure.
- 3. This Calibration is referenced to 0 Degrees Centigrade and 760 Torr.

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